

"Waste Water Recycling"
&
"Zero Liquid Discharge"



# **Zero Liquid Discharge**





In the end of the 1980's, together with increased environmental awareness within society and industry, "Zero discharge" changed from a technical description of 100% wastewater recycling to a "goal". The principle of "zero discharge" is recycling of all industrial wastewater.

This means that wastewater will be treated and used again in the process. Because of the water reuse wastewater will not be released on the sewer system or surface water.

# **Waste Hierarchy Pyramid**



Eliminate

Reduce

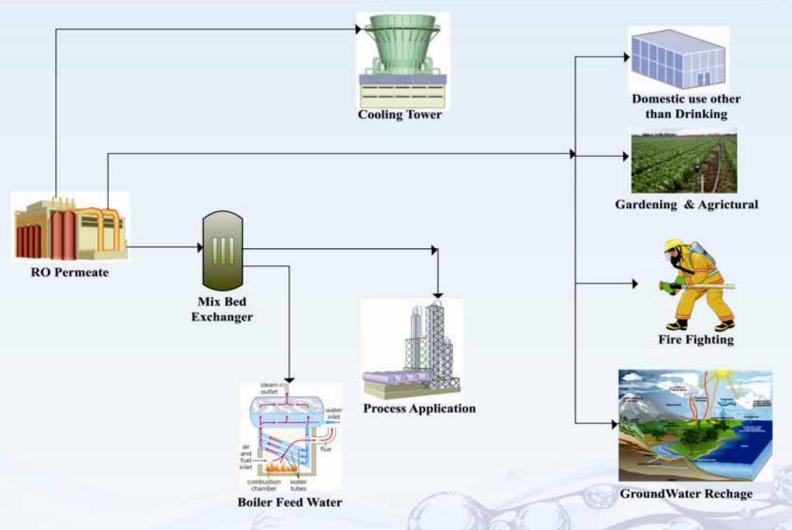
Reuse

Recycle

Dispose

# **Water Reuse Applications**





# **Waste Water Treatment**





- PRIMARY TREATMENTS
  COAGULATION / FLOCCUALTION
  THROUGH:
- SOLID CONTACT REACTOR / HRSSC
- PARALLEL PLATE / TUBE SETTLERS
- DISSOLVED AIR FLOATATION



- ACTIVATED SLUDGE PROCESS
  - ANAEROBIC REACTOR
  - ATTACHED GROWTH AEROBIC BIOLOGICAL SYSTEM
  - MBR

# **Technologies – Primary Treatment**





Clarifier



Clariflocculator



Solid contact clarifier



**Tube settler** 



**Dissolved Air Floatation** 



Oil skimmer



High Speed Clarifiers - MULTIFLO/ PULSATOR

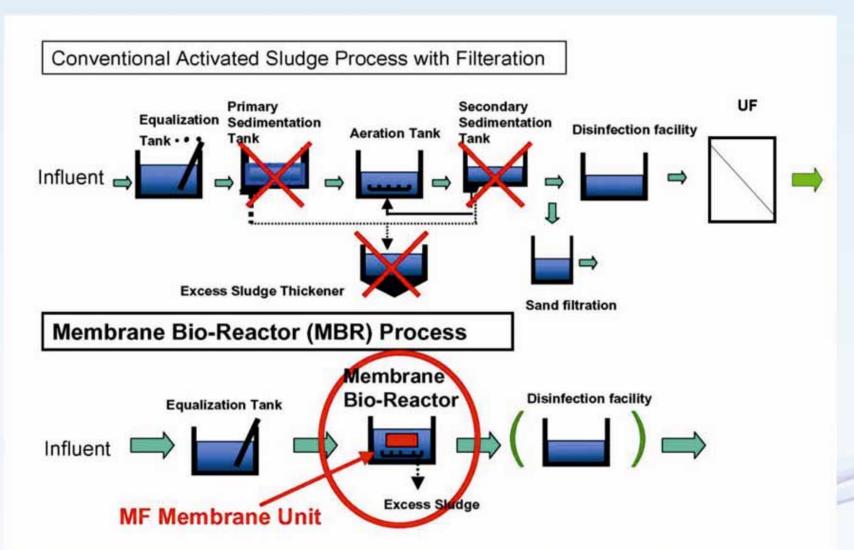
## Waste Water Treatment techologies - Secondary Treatment



- ASP (Activated Sludge Process with floating Aeration)
- MBBR (Moving Bed Bio Reactor)
- ASBR (Advanced Sequence Batch Reactor)
- MBR (Membrane Bio Reactor)

# **Membrane Bio Reactor (MBR)**



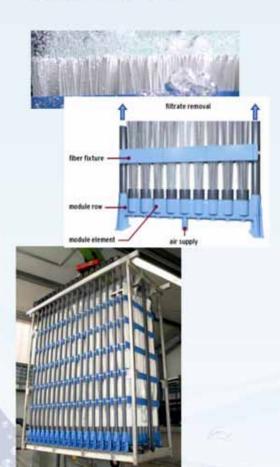


# Membrane types



Three main membranes Technologies are available in the market

#### **Hollow Fibers**



## External Tubular Membranes



## Flat Sheet Membranes



# **MBR** Configurations

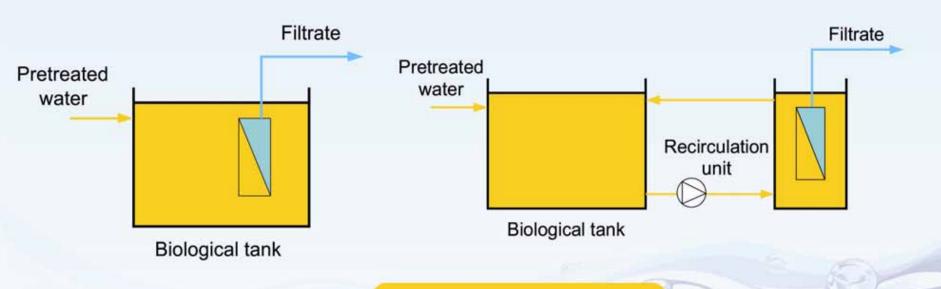


Two configurations according to the existing site constraints, the type of membrane selected & the design criteria.

Submerged System: Membrane immersed within the Biological reactor

or

External MBR: Membrane installed in a separated tank



Two MBR
Configurations to fit
all wastewater applications

# **Advantages of MBR**



## Quality

Disinfection, No Bacteria No SS nor colloids Biodegradable COD removed

#### Robust

No Bulking sludge No sludge loss Load Adjustment

#### **Water Reuse**

Direct irrigation
Perfect RO Pre-treatment

## Compactness

High sludge concentration Aeration Volume 1/3 of conventional No primary settler









Advantages Of MBR



## Neighbourhood

Closed system Odour control No open water surface







## **Flexibility**

Large operating window Easy modular extension

## **Simplicity**

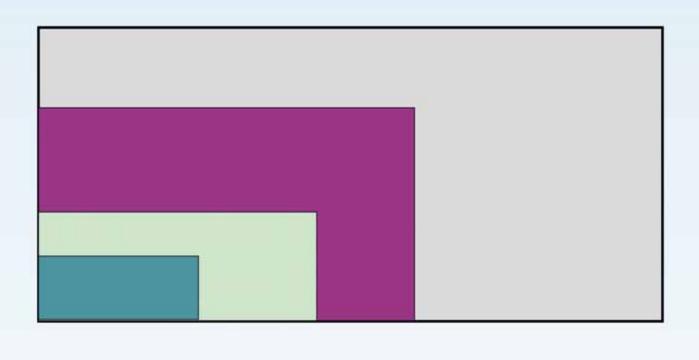
Hydraulic is simple Low pressure membranes

## Refurbishment

Use of existing plant Is easier and less costly

# **Area Requirement for ETP**





MBR



MBBR

**ACTIVATED SLUDGE PROCESS** 

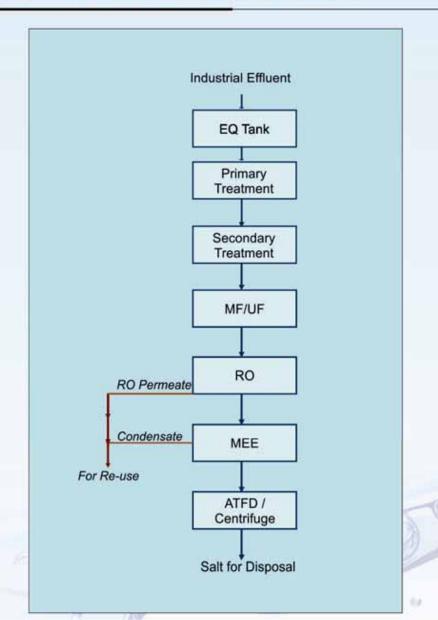
# Comparison of Waste Water Technologies PARAMOUNT



	MBBR	ASP	ASBR	MBR	
Biomass type	Fixed to plastic suspended carriers	Free biomass suspended in water	Free biomass suspended in water	Free biomass suspended in water	
Recommended Technology	Space constraint & upgradation of existing ETP. For horticulture.	Space available & skilled operation not required. For safe discharge	Load fluctuation & treated quality for horticulture	Recycle & reuse of treated effluent	
Operation & Maintenance	Medium skilled	Unskilled	Skilled	Highly Skilled	
Solids inlet sensibility	No. 3-5 mm screening necessary	No	No	Yes. 1mm screening necessary	
Flow variations sensibility	Yes. Limited to 2 <sup>nd</sup> clarifier capacity	Yes. Limited to 2 <sup>nd</sup> clarifier capacity	No	Yes. Buffer tank needed	
MLSS (g/I)	5-7	3-5	4-6	10 – 12	
Treated effluent quality (ppm)	TSS: 50 BOD: 20	TSS: 100 BOD: 30 – 50	TSS: 20 – 40 BOD: 10 - 20	TSS: BDL BOD < 5	

# **Typical Flow Chart for ZLD**





# **The Membrane Tertiary Treatment Solution**













**HGIW** 



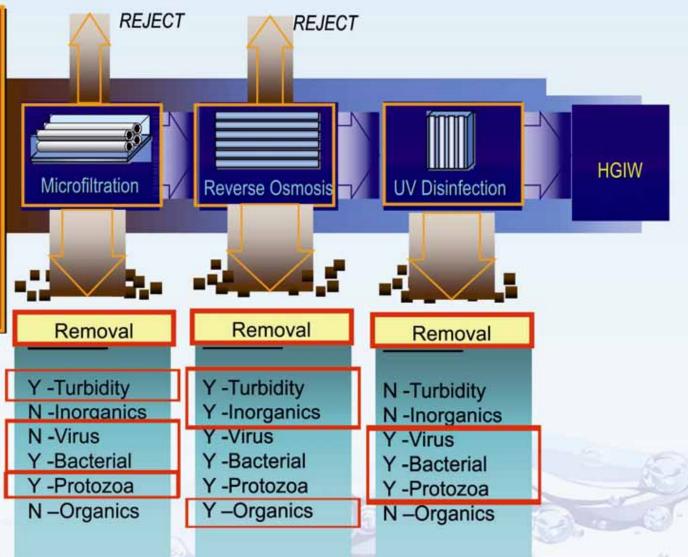
**UltraViolet** 

# **The Membrane Tertiary Treatment Solution**





- <sub>n</sub> Turbidity
- n Inorganics
- n Virus
- <sub>n</sub> Bacteria
- n Protozoa
- n Organics



# MF/UF Technologies Available in the Market Today



# Submerged

## VS

# Pressurised





# MF/UF Technologies Available in the Market Today



## Microporous hollow fibers

	$A_{m}$	$B_z$	C <sub>a</sub>	D <sub>h</sub>	En
<b>公司</b> 大力	Submerged		Pressurised		
	MF	UF	MF	UF	UF
Mode of operation	Dead-end		Cross-flow	Dead-end	
Filtration	Outside - In			Inside - out	
Membrane material	PP PVDF		DF	PES	
Pore size (um)	0.2	0.02	0.1	0.025	
Fiber orientation	Vertical	Horizontal	Vert	ical	Horizontal
Backwash	WATER				

## MicroFiltration (MF) Membrane System Design







## <u>Performance</u>

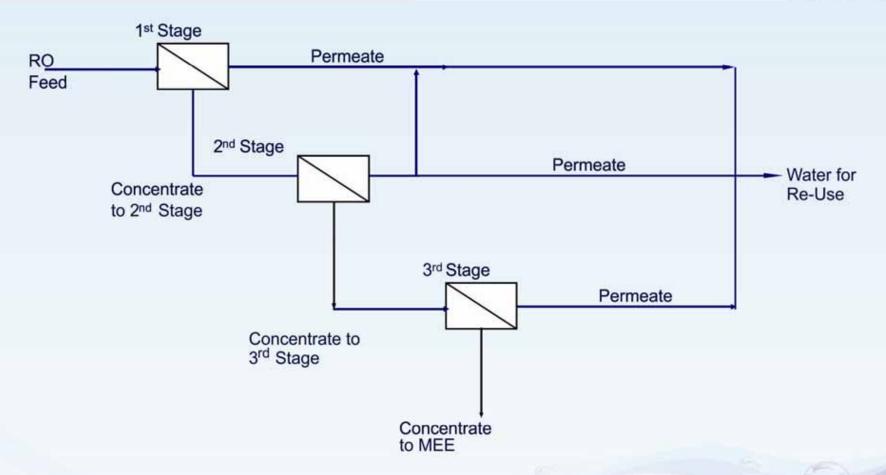
- Design Flux: approx. 33l/m2.h
- Recovery: 90% (min)
- Filtrate SDI: < 3.0</p>
- Filtrate Turbidity: < 0.5 NTU</p>

## Configuration (for submerged)

- 13 to 14 Membrane trains/Cells
- 14 racks/ train: 32 sub-modules/rack

# **Typical RO Membrane Systems – PFD**





Combination to achieve maximum recovery subject to inlet conditions.

# **Purpose of Evaporation**



- To concentrate solution by removing the vapor from a boiling liquid solution
- In the majority of cases, evaporation refers to the removal of water from an aqueous solution.
- Example: concentration of aqueous solutions of sugar, sodium chloride, sodium hydroxide, glycerol, glue, milk & orange juice. Apart from this now a days MEE is used to achieve the Zero Liquid discharge.
- In all the process application the concentrated solution is the desired product and in case of ZLD the condensate is desired product.
- In a few cases, water, which contains a small amount of minerals, is evaporated to give a solids-free water to be used as boiler feed, for special chemical processes.
- Evaporation processes to evaporate seawater to provide drinking water have been developed and used.

# **Processing Factors**



- Concentration in the liquid
  - low viscosity: high mass transfer coefficient
  - high viscosity: low mass transfer coefficient
  - adequate circulation and/or turbulence must be present to keep the coeffeicient from becoming too low
- Solubility
  - solubility increases with temperature
  - crystallization may occur when a hot concentrated solution is cooled to room temperature
- Temperature sensitivity of materials
  - food and biological materials may be temperature sensitive and degrade at higher temperature or after prolonged heating.

# **Processing Factors**



- Foaming or frothing
  - food solution such as skim milk and some fatty-acid solution form a foam or froth during boiling.
- Pressure and temperature
  - high operating pressure: high boiling point
- Scale deposition and materials of construction
  - Some solutions deposit solid materials called scale on the heating surfaces.
  - results in the overall heat-transfer coefficient decreases and evaporator must be cleaned.

# **Methods of Operation of Evaporators**



- Single-effect evaporators
- Forward-feed multiple-effect evaporators
- Backward-feed multiple-effect evaporators
- Parallel-feed multiple-effect evaporators

# Single-effect evaporators

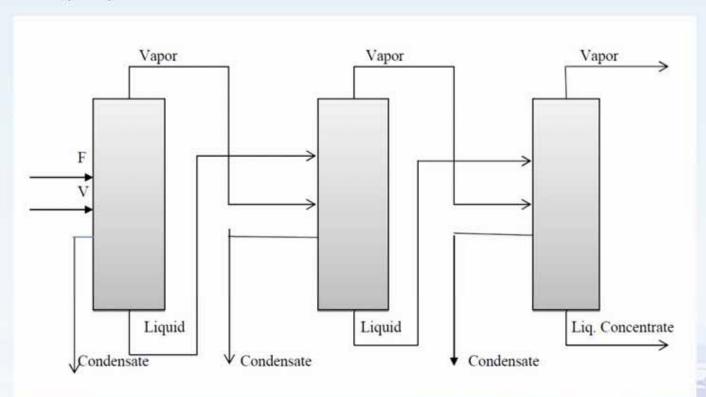


- Single-effect evaporators are often used when the required capacity of operation is relatively small and/or the cost of steam is relatively cheap compared to the evaporator cost.
- However, for large-capacity operation, using more than one effect will markedly reduce steam costs.

## **Forward Feed - MEE**



FORWARD FEED ARRANGEMENT: In this arrangement the feed and steam is introduced in the first effect. Pressure in the first effect is highest and pressure in last effect is minimum, so transfer of feed from one effect to another can be done without pump.



Forward feed arrangement in Multi effect Evaporator

# Forward-feed multiple-effect evaporators



- If the feed to the first effect is near the boiling point at the pressure in the first effect, 1kg of steam will evaporate almost 1 kg of water.
- The first effect operates at a temperature that is high enough that the evaporated water serves as the heating medium to the second effect.
- Here, again, almost another kg of water is evaporated, which can then be used as the heating medium to the third effect.
- As a very rough approximation, almost 3 kg of water will be evaporated for 1 kg of steam in a three-effect evaporator.
- Hence, the steam economy, which is kg vapor evaporated/kg steam used, is increased.
- This also holds approximately for more than three effects.
  - However, the increased steam economy of a multiple-effect evaporator is gained at the expense of the original first cost of these evaporators.

# Forward-feed multiple-effect evaporators

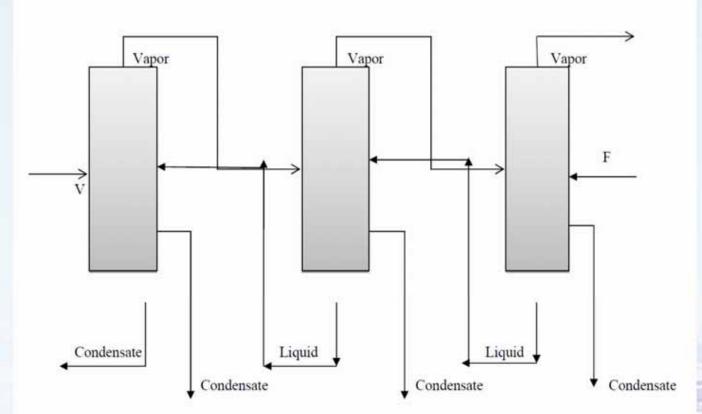


- In forward-feed operation the fresh feed is added to the first effect and flows to the next in the same direction as the vapor flow.
- This method of operation is used when the feed is hot or when the final concentrated product might be damaged at high temperatures.
- The boiling temperatures decrease from effect to effect.
   This means that if the first effect is at P1 = 1 atm abs pressure, the last effect wilt be under vacuum at a pressure P3.

## **Backward Feed - MEE**



BACKWARD FEED ARRANGEMENT: In this arrangement feed is introduced in last effect and steam is introduced in first effect. For transfer of feed, it requires pump since the flow is from low pressure to higher pressure. Concentrated liquid is obtained in first effect.



**Backward feed arrangement in Multi effect Evaporator** 

# **Backward-feed multiple-effect evaporators**



- In the backward-feed operation for a triple-effect evaporator, the fresh feed enters the last and coldest effect and continues on until the concentrated product leaves the first effect.
- This method of reverse feed is advantageous when the fresh feed is cold, since a smaller amount of liquid must be heated to the higher temperatures in the second and first effects.
- However, liquid pumps must be used in each effect, since the flow is from low to high pressure.
- This reverse-feed method is also used when the concentrated product is highly viscous.
- The high temperatures in the early effects reduce the viscosity and give reasonable heat-transfer coefficients.

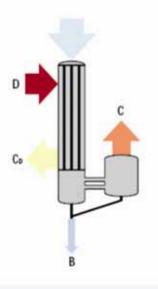
# **Types of Vapour Recompression**

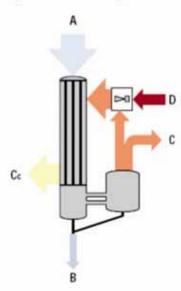


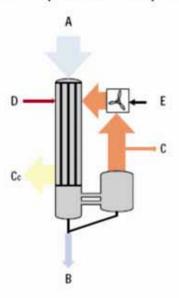
## Directly heated

Thermal vapour recompressor

Mechanical vapour recompressor







A: Product

B: Concentrate

C : Vapour

D: Steam

E: Electrical energy

Cc: Steam condensate

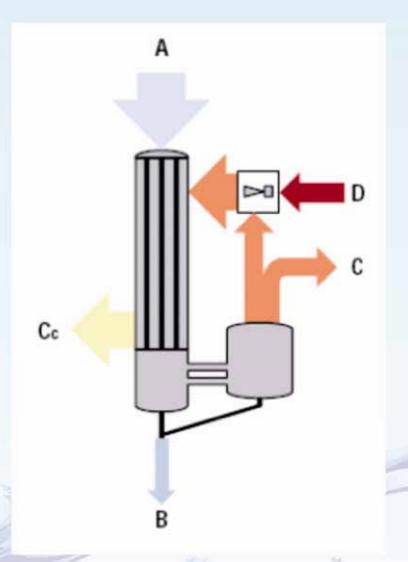
# **Thermal Vapour Recompressor**



During thermal vapour recompression, vapour from a boiling chamber is recompressed to the higher pressure of a heating chamber according to the heat pump principle; i.e. energy is added to the vapour.

For this purpose, thermal vapor recompressor are used.

A certain quantity of live steam, the so-called motive steam, is required for the operation of a thermal vapour recompressor. This motive steam quantity must be transferred to the next effect or to the condenser as surplus residual vapour. The surplus energy contained in the residual vapour approximately corresponds to the amount of energy supplied in the motive steam.



# **Mechanical Vapour Recompressor**



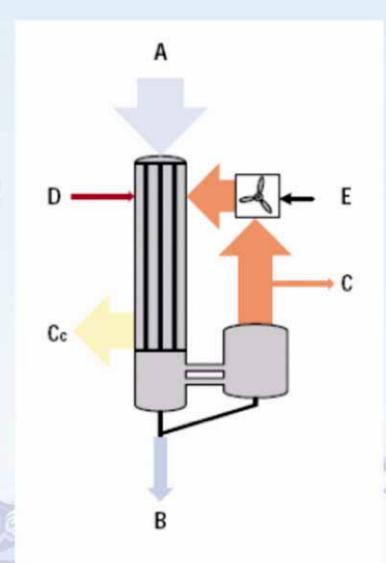
In mechanical vapor compression, positive displacement compressors or multi stage centrifugal compressors are generally used to raise the pressure and temperature of the generated vapors.

Since mechanical compressors do not require any motive steam, all vapors can be compressed to elevated pressure and temperature eliminating the need for subsequent recovery system.

After compression of vapor and subsequent condensation of the same, hot condensate leaves the system.

The main features of MVR are as follow:

- \* Most energy efficient evaporation technology (n-effect)
- \* Flexible and simple to use
- \* Generally single effect (reduced footprint)
- \* No steam and cooling water consumption (boiler and cooling tower cost reduction)
- \* Suitable for moderate boiling elevation products Low specific operating cost





# Case Studies Waste Water Recycle &

Zero Liquid Discharge



# **Swil Copper Ltd**

Flow: 225 m3/day

(Copper Smelter)

# **ZLD Using Evaporative Cooling & Waste Gases**

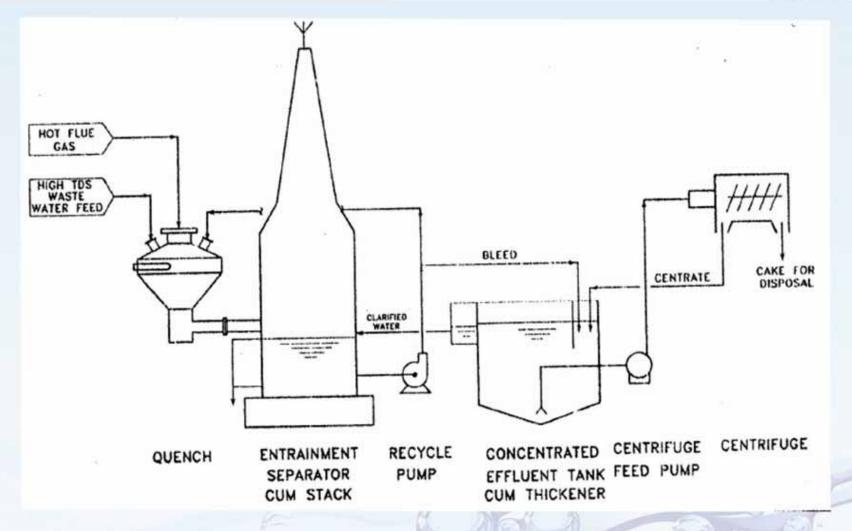


## "Paramount's Innovative approach to zero discharge using "Quench"

## Paramount Design- Technical Approach

- Paramount offers a system that uses the concept of evaporative cooling. But it is looked at from a different perspective. In normal practice,
- A Quench is used to cool the hot gas by having a direct contact water spray to reduce the gas temperature. Water is evaporated and converted to steam which is based on evaporative cooling.
- But in case of Paramount's design of Quench for concentrating the high TDS bearing waste water,
- Quench is used to evaporate the water using waste water heat rather than the conventional concept of cooling the gases with water.







This concept was used at M/S SWIL for evaporating water from waster containing high level of dissolved solids using waste heat in the flue gases from power plant and resulted in:

- Concentration of the waste water in the form of slurry containing suspended solids, generated due to presence of high TDS (50000-55000 ppm) and evaporation of water which is centrifuged to form a disposable cake.
- The centrate from the centrifuge is sent back to the quenching system for further evaporation and cooled gases with water vapour is discharged to atmosphere through stack.



Inlet treated effluent : 130-225 m³/day

TDS : 33,000-53,000 ppm

pH : 7-8



#### **Conclusion**

- This concept was found highly feasible and practical solution for evaporation of waste water to achieve zero discharge goal.
- This concept was also presented to Ministry of Environment and forest and has been accepted.
- This approach also helps to achieve reduction in the initial cost of the plant including extremely low operating cost.



## **Mangalore Refinery**

Flow: 24000 m3/day

(Refinery & Petrochemical Industry)

#### **MRPL Charactristics**



Average

combined

milet emanacteristics	Inlet	Chara	cteristics
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mict onaracteristics	2	stream after UF		feed to RO
Parameter	Units	Concentration	Concentration	Concentration
Total Suspended Solids	mg/l	< 1	< 5	< 3.4
TDS	mg/l	2049	1200	1540
BOD 27°C, 3 days	mg/l	4	< 3	< 3.4
COD	mg/l	17	< 20	19
M Alkalinity	mg/l	100	300	220
Calcium Hardness as CaCO <sub>3</sub>	mg/l	226	85	141
Magnesium Hardness as CaCO <sub>3</sub>	mg/l	126	55	83.4

CTBD & DM

neutralized

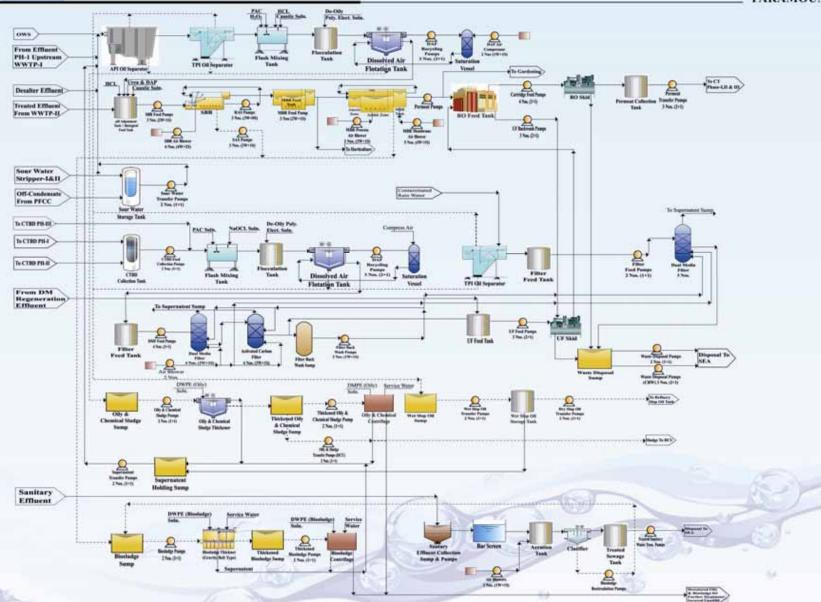
From MBR

#### **Outlet Characteristics**

Parameter	Un	its	Concentration	
Total Suspended Solids	mç	g/I	Nil	
TDS	mç	g/I	80	
BOD 27°C, 3 days	mç	J/I	BDL	
COD	mg	<b>J</b> /l	BDL	
M Alkalinity	mg	g/l	10	15
Calcium Hardness as CaCO <sub>3</sub>	mg	<b>y/I</b>	5	
Magnesium Hardness as CaCO <sub>3</sub>	mg mg	3/1	3	_(8)
Operating Cost	Rs		27/m3	0

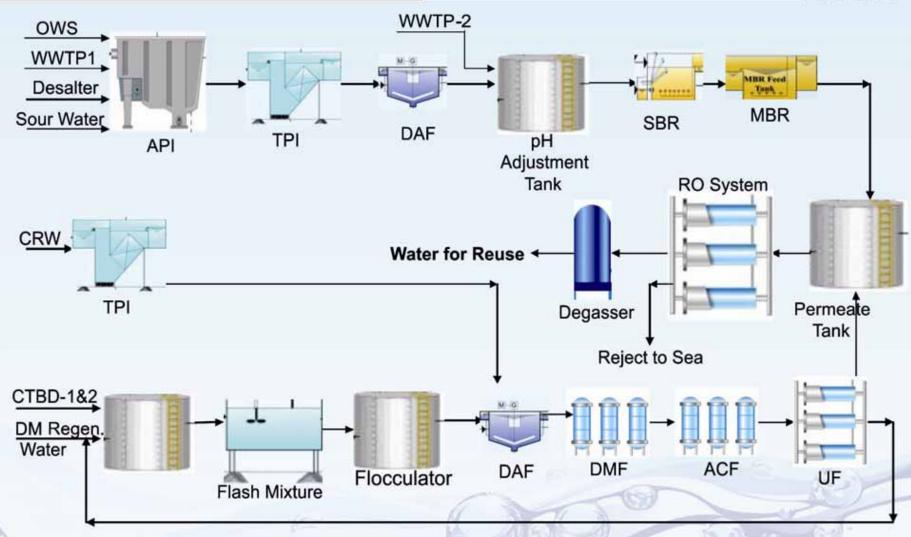
#### **MRPL** - Chart





#### **Block Diagram MRPL**





#### **MRPL** - Site









**TPI Unit** 

**API** Unit

**DAF** Unit



SBR Unit



MBR Unit



DMF - ACF Filter

#### **MRPL** - Site









Control Room

**Chemical House** 

RO Skid







**RO** Degasser

Micron Filter

Over All View



# Chennai Petroleum Corporation Ltd

Flow: 10,000 m3/day

(Petrochemical Industry)

#### **CPCL Charactristics**



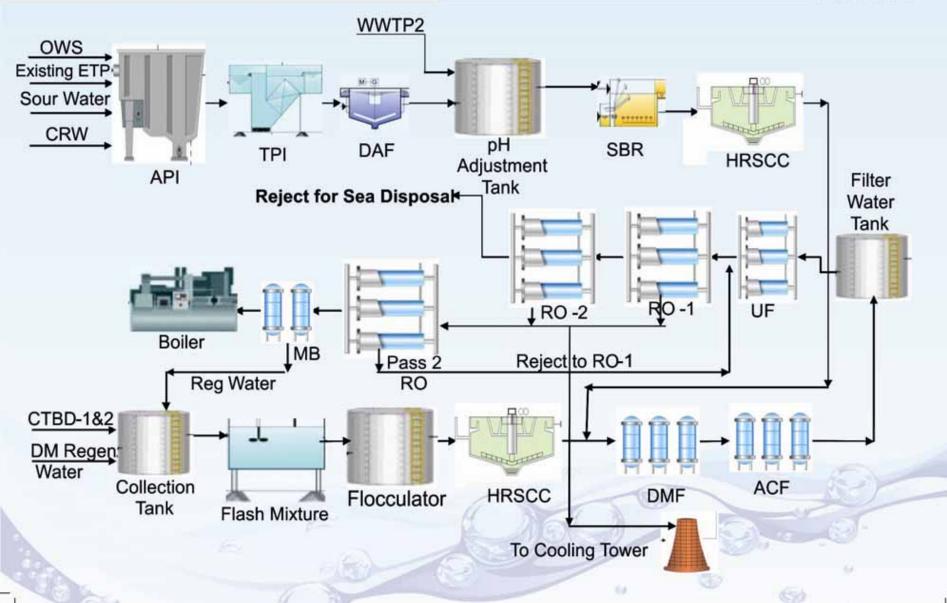
<b>Inlet Characteristics</b>		neutralized stream after UF	From SBR	combined feed to RO	
Parameter	Units	Concentration	Concentration	Concentration	
Total Suspended Solids	mg/l	< 1	< 5	< 3	
TDS	mg/l	4000	1500	2500	
BOD 27°C, 3 days	mg/l	5	< 5	< 5	
COD	mg/l	20	< 20	20	
M Alkalinity	mg/l	100	300	220	
Calcium Hardness as CaCO <sub>3</sub>	mg/l	226	85	141	
Magnesium Hardness as CaCO <sub>3</sub>	mg/l	126	55	83.4	

#### **Outlet Characteristics after MB**

Parameter	Units	Concentration	1
Total Suspended Solids	mg/l	Nil	
TDS	mg/l	< 1	
BOD 27°C, 3 days	mg/l	BDL	
COD	mg/l	BDL	
Silica	mg/l	0.02	
Operating Cost	Rs.	45/m3	

#### **Block Diagram CPCL**





#### **RO Skid at Paramount Workshop**





RO Skid



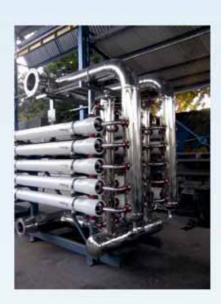
RO Skid

#### **UF Skid at Paramount Workshop**











## **Pigment Industry**

Flow: 1000 m3/day

Client-1: Asahi Songwon India Ltd

Client-2: Meghmani Organics Ltd

#### **Pigment Industry**



**Inlet Characteristics** 

Color : Light Blue

Design TDS : 10000 PPM

TSS : 250 PPM

COD : 1000 PPM

BOD : 250 PPM

Ammonical Nitrogen : 450 PPM

**Outlet Characteristics** 

Recovery : 82% (3 Stage System)

Operating Cost : Rs.53/m3

Permeate TDS : <500 PPM

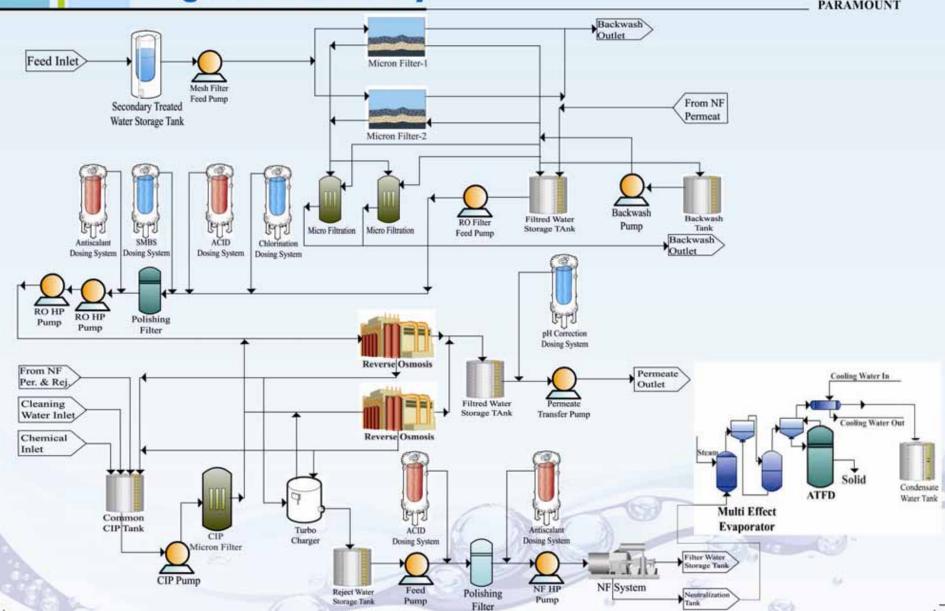
Permeate COD : <50

Permeate Color : Color less

Ammonical Nitrogen : <50 PPM

#### **Pigment Industry**





## Pigment Industry-Ceramic Micro Filtration PARAMOUNT















## **Sanofi Aventis**

Flow: 300 m3/day

(API / Bulk Drug Industry)

#### **Sanofi-Aventis Ltd**



**Inlet Characteristics** 

Design TDS : 3000 PPM

COD : 600 PPM

BOD : 100 PPM

**Outlet Characteristics** 

Recovery : 85%( 2 Stage RO system)

Operating Cost : Rs.30/m3

Permeate TDS : <250 PPM

Permeate COD : <30

Permeate Color : Color less

#### **Sanofi-Aventis Ltd**



#### **Inlet Characteristics (MEE)**

Design TDS : 4% to 14%

COD : 20000 PPM

#### **Outlet Characteristics**

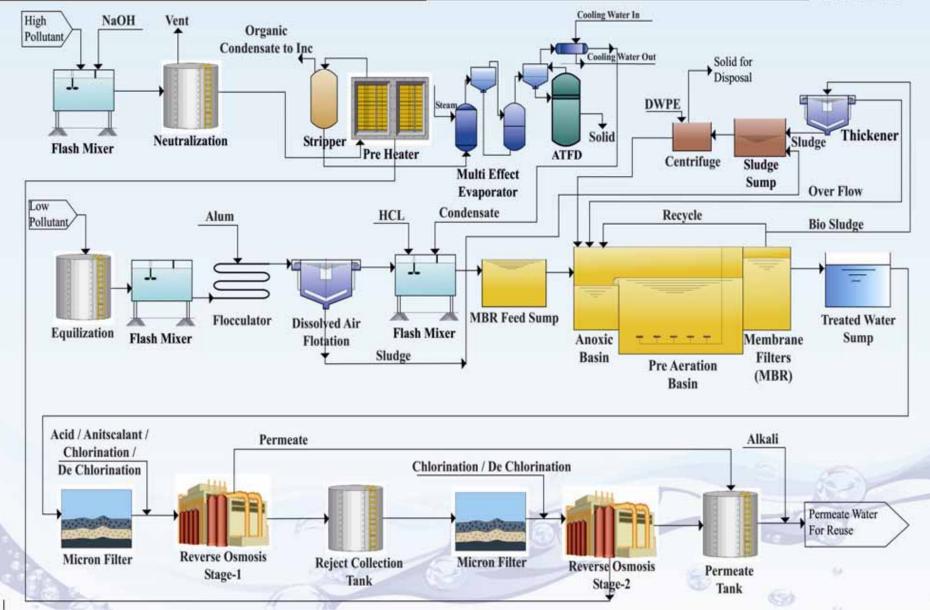
Condensate TDS : <500 PPM

Condensate COD : <3000 PPM

Operating Cost : Rs.625/m3

#### Sanofi - Aventis





#### Sanofi - Aventis - Site











#### Sanofi - Aventis - Site













## Sandoz

Flow: 400 m3/day

(Pharmaceutical Industry)

#### Sandoz



#### **Inlet Characteristics**

Design TDS : 3000 PPM

COD : 250 PPM

BOD : 75 PPM

#### **Outlet Characteristics**

Recovery : 85% (2 stage system)

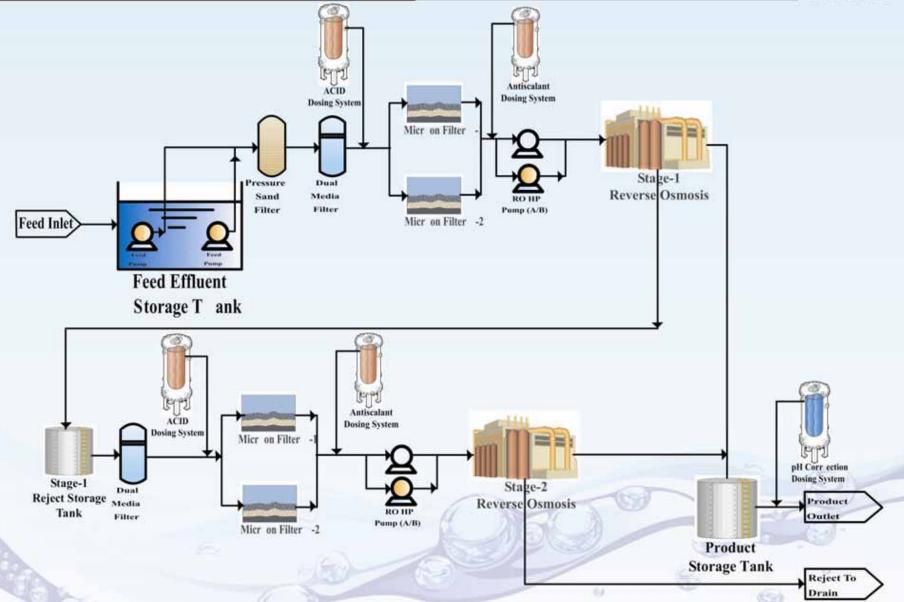
Operating Cost : Rs.30/m3

Permeate TDS : <250 PPM

Permeate COD : <15

#### Sandoz





#### Sandoz ETP - Reuse





Scheme: Iron Removal Filter – DMF – Dosing System – MCF – 1st Stage RO – Dosing Sys for 2nd stage – MCF - 2nd Stage RO – post pH Correction.

- Client : Sandoz, Mumbai.
- Capacity : 400 m³/day System Recovery 85%





## Ess Kay Yarn

Flow: 50 m3/day

(Textile Dyeing Industry)

#### **Ess Kay Yarn (Textile Industry)**



Capacity of plant : 50 m3/day

Color : Dark Blue

Design TDS : 22000 PPM

COD : 9000 PPM

BOD : 3500 PPM

Recovery : 50%(3<sup>rd</sup> Stage system)

Operating Cost : Rs.40/m3

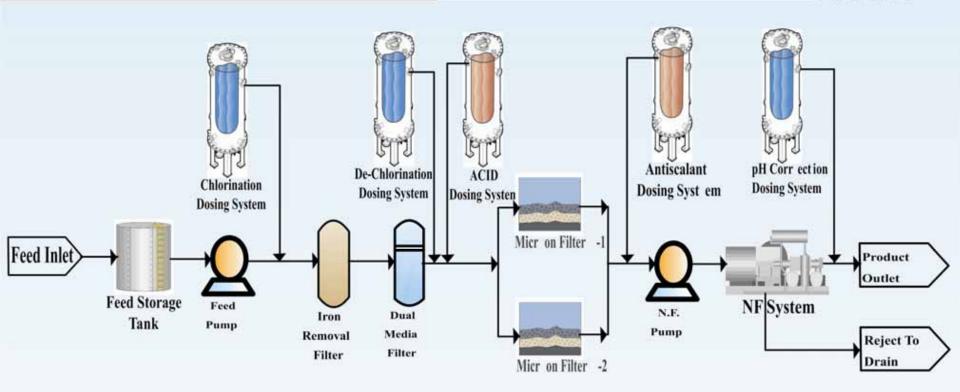
Permeate TDS : <500 PPM

Permeate COD : <50

Permeate Color : Color less

#### **Ess Kay Yarn**





#### **Ess Kay Yarn**





RO Skid



RO Skid



### Mazda Colors

Flow: 500 m3/day

(Color & Pigment Industry)

#### **Mazda Colors**



**Inlet Characteristics** 

Design TDS : 5000 PPM

COD : 600 PPM

BOD : 100 PPM

**Outlet Characteristics** 

Recovery : 75%

Operating Cost : Rs.32/m3

Permeate TDS : <250 PPM

Permeate COD : <30

Permeate Color : Color less

#### **Mazda Colors**



#### **Inlet Characteristics (MEE)**

Design TDS : 4%

COD : 30000 PPM

#### **Outlet Characteristics**

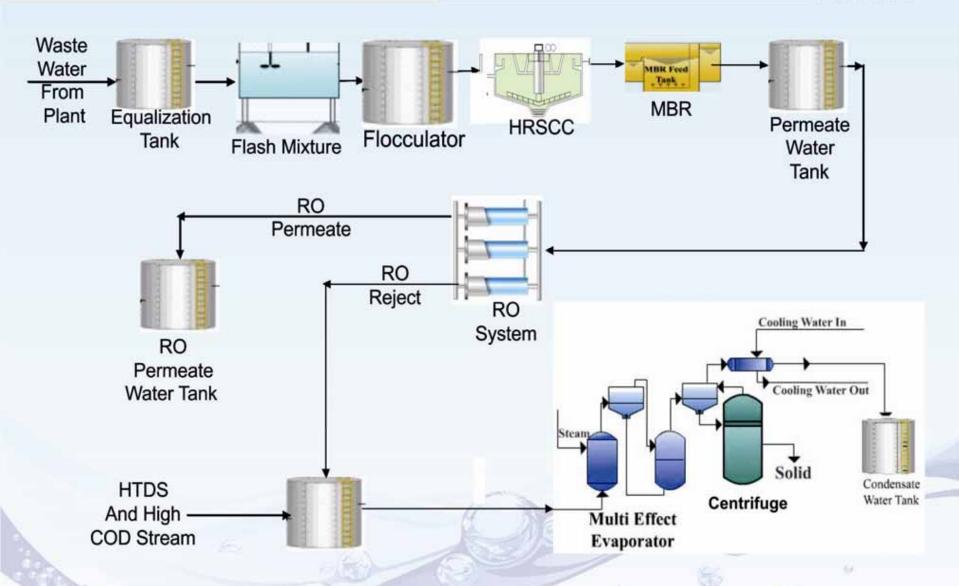
Condensate TDS : <100 PPM

Condensate COD : <50 PPM

Operating Cost : Rs.660/m3

#### **Block Diagram Mazda Colors**





#### **Mazda Colors - Site**









## Micro Inks

Flow: 1500 m3/day

(Ink Manufacturing Unit)

#### **Micro Inks**



#### **Inlet Characteristics**

Design TDS : 5000 PPM

COD : 1500 PPM

BOD : 400 PPM

#### **Outlet Characteristics**

Recovery : 85% (2 stage & 2 Pass system)

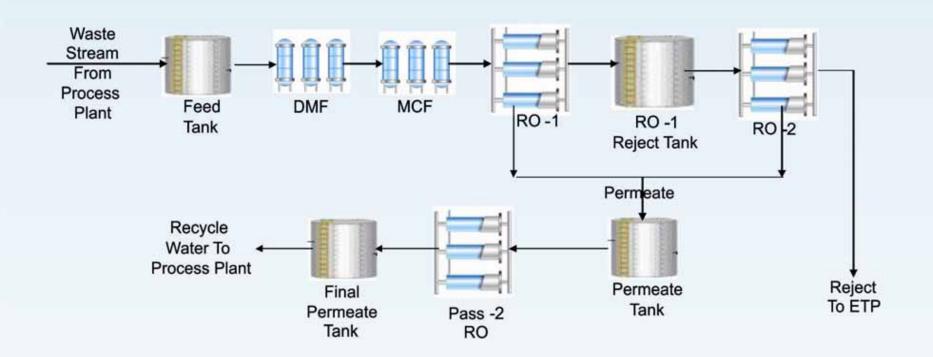
Operating Cost : Rs.40/m3

Permeate TDS : <100 PPM

Permeate COD : <15

#### **Block Diagram Micro Inks**







## Anubha Fabrics Pvt. Ltd.

Flow: 600 m3/day

(Yarn Manufacturing Unit)

#### **Anubha Fabrics Pvt. Ltd**



**Inlet Characteristics** 

Design TDS : 1500 PPM

COD : 300 PPM

BOD : 100 PPM

Oil : 100 PPM

**Outlet Characteristics** 

Recovery : 75%

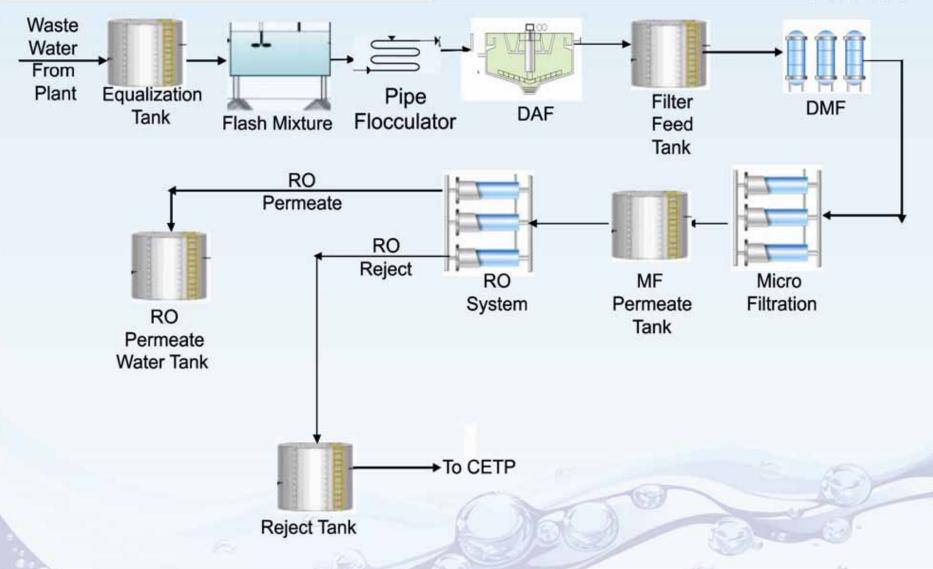
Operating Cost : Rs.35/m3

Permeate TDS : <100 PPM

Permeate COD : <10

#### **Block Diagram Anubha Fabrics Pvt. Ltd**





## Thank You



#### PARAMOUNT LIMITED

(Formerly Paramount Pollution Control Limited) (An ISO 9001 Company)

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